## Principles of Humidity - Dalton's law

Air is a mixture of different gases. The main gas components are:

| Gas component | volume [\%] | weight [\%] |
| :---: | :---: | :---: |
| Nitrogen $\mathrm{N}_{2}$ | 78,03 | 75,47 |
| Oxygen $\mathrm{O}_{2}$ | 20,99 | 23,20 |
| Argon Ar | 0,93 | 1,28 |
| Carbon dioxide $\mathrm{CO}_{2}$ | 0,03 | 0,04 |
| Rest: $\mathrm{H}_{2}, \mathrm{Ne}, \mathrm{He}, \mathrm{Kr}$ | 0,02 | 0,01 |

On normal physical conditions these gases behave ideal which means that the gas molecules act independent from each other which leads to Dalton's law :
"The total pressure of a gas is the sum of the pressures of each component"
The pressure of a single component is called partial pressure, so the total pressure of air is the sum of the partial pressures of its components i.e.

$$
\begin{gathered}
\mathrm{p}=\mathrm{p}_{\mathrm{N} 2}+\mathrm{p}_{\mathrm{O} 2}+\mathrm{p}_{\mathrm{Ar}}+\ldots \\
\text { dimension of } \mathrm{p}:[\mathrm{mbar}] \text { or }[\mathrm{hPa}]
\end{gathered}
$$

Water in its gaseous phase (vapour) is an additional ideal gas component of air which appears in Dalton's law :

$$
\mathrm{p}=\mathrm{p}_{\mathrm{N} 2}+\mathrm{p}_{\mathrm{O} 2}+\mathrm{p}_{\mathrm{Ar}}+\ldots+\mathrm{e}=\mathrm{p}_{\mathrm{da}}+\mathrm{e}
$$

e partial pressure of (water) vapour [mbar]
$\mathrm{p}_{\mathrm{da}} \quad$ partial pressure of dry air

## Principles of Humidity - Vapour pressure

## Vapour pressure above water

Vapour pressure cannot take on any value in air. There is a maximum partial pressure of vapour which depends only on air temperature. At high temperatures air can hold more vapour than at low temperatures.

This behaviour can be explained in the following way :
The molecules, bounded in a liquid like water, are moving with different velocities and the average kinetic energy is proportional to the temperature of the liquid. The energy distribution of the molecules is statistical as shown in Fig.1.


Fig. 1: Statistical energy distribution of molecules in a liquid at different temperatures.

The overall average kinetic energy of the molecules is depending on temperature whereas the energy of a single molecule can be lower or higher with a statistical probability. Molecules with energies below the binding energy of the liquid cannot leave the water surface, but some have enough energy to exceed the binding force. These molecules can leave the liquid, they evaporate from the water surface and increase the vapour concentration in the room above the water surface.

The molecules in the vapour behave similar but for them the case to have less energy than the binding energy of water is exceptional: they are absorbed from the water surface by condensation and decrease the vapour concentration.

A closed box partly filled with water at temperature t (Fig.2) will stabilize in equilibrium between evaporation and condensation. If there is a lack of water molecules in the moist region, more evaporation will occur and the vapour concentration will increase. In the opposite case more molecules will condense than evaporate and the vapour concentration will decrease.


Fig. 2 : Box partly filled with water at constant temperature
The balance between evaporation and condensation leads to a vapour pressure, which depends only on temperature. Increasing the temperature more molecules have higher energies (see Fig.1), will leave the water surface and shift the equilibrium to higher vapour concentrations.

On normal environmental conditions vapour is an ideal gas with no interaction with other present ideal gases. So the vapour concentration is practically independent from other existing gases in the region above the water surface.

In the box at temperature $t$ the balanced vapour pressure is a maximum at this temperature and is called
"saturation vapour pressure" above water $\mathrm{e}_{\mathrm{w}}$ at temperature t .
The saturation pressure above water $\mathrm{e}_{\mathrm{w}}$ depends approximately exponential on temperature t . Values for $e_{w}$ for different temperatures are given in Tab. $1{ }^{[1]}$.

| $\mathbf{t}$ [degC] | $\mathbf{e}_{\mathbf{w}}$ [mbar] | $\mathbf{t}$ [degC] | $\mathbf{e}_{\mathbf{w}}$ [mbar] |
| :---: | :---: | :---: | :---: |
|  |  |  |  |
| 100 | 1014.19 | 0 | 6.112 |
| 90 | 701.82 | -10 | 2.8652 |
| 80 | 474.16 | -20 | 1.2559 |
| 70 | 312.02 | -30 | 0.5103 |
| 60 | 199.48 | -40 | 0.1903 |
| 50 | 123.53 | -50 | 0.0644 |
| 40 | 73.853 | -60 | 0.0195 |
| 30 | 42.470 | -70 | $5.187 \mathrm{E}-03$ |
| 20 | 23.392 | -80 | $1.190 \mathrm{E}-03$ |
| 10 | 12.281 | -90 | $2.298 \mathrm{E}-04$ |
| 0.01 | 6.117 | -100 | $3.622 \mathrm{E}-05$ |

Tab. 1: Saturation vapour pressure values $\mathrm{e}_{\mathrm{w}}$ above water

## Vapour pressure above ice

Below $t=0.01$ degC (triple point of water) water can exist in the liquid phase as well as in the solid phase (ice) but the liquid phase is usually not stable. The physical interpretation of evaporation above ice is equal to water.

| $\mathbf{t}$ [degC] | $\mathbf{e}_{\mathbf{i}}$ [mbar] |
| :---: | :---: |
|  |  |
| 0.01 | 6.117 |
| 0 | 6.112 |
| -10 | 2.5989 |
| -20 | 1.0324 |
| -30 | 0.3800 |
| -40 | 0.1284 |
| -50 | 0.0394 |
| -60 | 0.0108 |
| -70 | $2.615 \mathrm{E}-03$ |
| -80 | $5.472 \mathrm{E}-04$ |
| -90 | $9.670 \mathrm{E}-05$ |
| -100 | $1.402 \mathrm{E}-05$ |

Tab. 2 : Saturation vapour pressure values $e_{i}$ above ice

According to the existence of a solid and liquid phase there are two saturation curves below $t=0.01$ degC as shown in Fig. 3 on a logarithmic scale. Mind that between - 100 degC and 100 degC the saturation vapour pressure is changing over 8 orders of magnitude!


Fig. 3 : Vapour saturation curves above ice and water. Below the triple point $(\mathrm{t}=0.01 \mathrm{degC})$ the curve splits into two graphs.

## Real gas correction

As so far water vapour was treated as an ideal gas i.e. water molecules act independent from the surrounding air. In reality there is an interaction between water molecules and the air which leads to a small increase of saturation vapour pressure under presence of air. This fact is taken into account by the enhancement factor $f(p, t)$.

The saturation vapour pressure under presence of air $e^{\prime}{ }_{w}$ is given by

$$
e^{\prime}{ }_{w}=e_{w}(t) \cdot f(p, t)
$$

At normal pressure ( $\mathrm{p}<1100 \mathrm{mbar}$ ) the enhancement factor is close to one and can usually be neglected. This means that water vapour mostly behaves like an ideal gas.

If you wish higher accuracies you should correct the saturation water pressure using the enhancement factor f , which depends on air pressure p and temperature t (for values see Tab. $3^{[2]}$ ).

| $\mathbf{t}$ [degC] | $\mathbf{- 4 0}$ | $\mathbf{- 2 0}$ | $\mathbf{0}$ | $\mathbf{1 0}$ | $\mathbf{2 0}$ | $\mathbf{3 0}$ | $\mathbf{4 0}$ | $\mathbf{6 0}$ | $\mathbf{8 0}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\mathbf{p}$ [bar] |  |  |  |  |  |  |  |  |  |
| 0.25 | 1.0013 | 1.0012 | 1.00131 | 1.00148 | 1.00173 | 1.00202 | 1.00223 | 1.00111 |  |
| 0.5 | 1.0026 | 1.0022 | 1.00217 | 1.00229 | 1.00251 | 1.00284 | 1.00323 | 1.00362 | 1.00051 |
| 1 | 1.0052 | 1.0044 | 1.0039 | 1.00388 | 1.004 | 1.00426 | 1.00467 | 1.00571 | 1.00564 |
| 1.5 | 1.0078 | 1.0065 | 1.0056 | 1.0055 | 1.00547 | 1.00564 | 1.00599 | 1.00713 | 1.00801 |
| 2 | 1.0104 | 1.0086 | 1.0074 | 1.0071 | 1.0069 | 1.00701 | 1.00728 | 1.00839 | 1.00968 |
| 2.5 | 1.013 | 1.0108 | 1.0091 | 1.0087 | 1.0084 | 1.0084 | 1.0086 | 1.00959 | 1.01108 |
| 3 | 1.0156 | 1.0129 | 1.0108 | 1.0103 | 1.0099 | 1.0097 | 1.0098 | 1.0108 | 1.01234 |
| 3.5 | 1.0183 | 1.015 | 1.0126 | 1.0119 | 1.0114 | 1.0111 | 1.0111 | 1.0119 | 1.01351 |
| 4 | 1.0209 | 1.0172 | 1.0144 | 1.0135 | 1.0128 | 1.0125 | 1.0124 | 1.013 | 1.0146 |
| 4.5 | 1.0236 | 1.0194 | 1.0161 | 1.0151 | 1.0143 | 1.0138 | 1.0136 | 1.0142 | 1.0157 |
| 5 | 1.0262 | 1.0215 | 1.0179 | 1.0167 | 1.0158 | 1.0152 | 1.0149 | 1.0153 | 1.0168 |
| 10 | 1.0533 | 1.0435 | 1.0356 | 1.033 | 1.0308 | 1.029 | 1.0277 | 1.0265 | 1.0271 |
| 20 | 1.11 | 1.089 | 1.072 | 1.066 | 1.0615 | 1.0573 | 1.0539 | 1.0493 | 1.0474 |
| 30 | 1.171 | 1.138 | 1.111 | 1.101 | 1.093 | 1.087 | 1.081 | 1.073 | 1.068 |
| 40 | 1.237 | 1.189 | 1.151 | 1.138 | 1.126 | 1.117 | 1.109 | 1.096 | 1.089 |
| 50 | 1.307 | 1.243 | 1.193 | 1.175 | 1.161 | 1.148 | 1.137 | 1.121 | 1.111 |
| 60 | 1.38 | 1.3 | 1.237 | 1.215 | 1.196 | 1.18 | 1.167 | 1.146 | 1.133 |
| 70 | 1.46 | 1.36 | 1.282 | 1.256 | 1.233 | 1.213 | 1.197 | 1.172 | 1.155 |
| 80 | 1.55 | 1.42 | 1.33 | 1.298 | 1.271 | 1.248 | 1.228 | 1.198 | 1.178 |
| 90 | 1.64 | 1.49 | 1.381 | 1.343 | 1.311 | 1.284 | 1.261 | 1.226 | 1.202 |
| 100 | 1.75 | 1.56 | 1.43 | 1.389 | 1.352 | 1.32 | 1.294 | 1.254 | 1.226 |

Tab. 3 : Enhancement factor $\mathrm{f}(\mathrm{p}, \mathrm{t})$

## Principles of Humidity - Magnus formula

The saturation vapour pressure above ice and water can be calculated with good accuracy with the Magnus formula ${ }^{[1]}$ :

$$
e_{w, i}=A \exp \left(\frac{m \cdot t}{T_{n}+t}\right)
$$

The parameters $\mathrm{A}, \mathrm{m}, \mathrm{T}_{\mathrm{n}}$ are different for ice and water and are given in Tab. 4.

| Temperature range $\mathbf{t}[\mathbf{d e g} \mathbf{C}]$ | $\mathbf{A}$ | $\mathbf{m}$ | $\mathbf{T}_{\mathbf{n}}$ |
| :--- | :---: | :---: | :---: |
| above ice : -80 to 0.01 | 6.112 | 22.46 | 272.62 |
| above water : -45 to 50 | 6.112 | 17.62 | 243.12 |

Tab. 4 : Magnus formula parameter ${ }^{[1]}$

## Principles of Humidity - Relative humidity

## Relative humidity $\mathbf{U}_{\mathrm{w}}$ [\%]

Table 1 and 2 (in section "Vapour pressure") give values for the saturation water vapour pressure as a function of temperature. These values are maximum values, in practice partial vapour pressures are usually lower.

Relative humidity $\mathrm{U}_{\mathrm{w}}$ is defined as the ratio between the actual partial vapour pressure e and the saturation vapour pressure above water $\mathrm{e}_{\mathrm{w}}$

$$
U_{w}=\frac{e}{e_{w}} \cdot 100 \quad[\%]
$$

Since the partial vapour pressure cannot exceed the saturation vapour pressure, the maximum value of relative humidity is $\mathrm{U}_{\mathrm{w}}=100 \%$.

## Relative humidity below the triple point

The definition of relative humidity below the triple point of water $\mathrm{t}<0.01 \mathrm{degC}$ refers again to the saturation pressure above water. In this exceptional temperature regime you can either have water with saturation vapour pressure $e_{\mathrm{w}}$ or ice with a smaller value $\mathrm{e}_{\mathrm{c}}<\mathrm{e}_{\mathrm{w}}$. In most applications however you will find ice since this is the stable state for temperatures $t<0.01$ $\operatorname{degC}$. So the case $\mathrm{e}=\mathrm{e}_{\mathrm{i}}$ gives you an upper limit for the relative humidity:

$$
t<0.01^{\circ} \mathrm{C}: \quad U_{w, \text { max }}=\frac{e_{i}}{e_{w}} \cdot 100 \quad \text { [\%] }
$$

| $\mathbf{t}[\mathbf{d e g} \mathbf{C}]$ | $\mathbf{0}$ | $\mathbf{- 5}$ | $\mathbf{- 1 0}$ | $\mathbf{- 1 5}$ | $\mathbf{- 2 0}$ | $\mathbf{- 2 5}$ | $\mathbf{- 3 0}$ | $\mathbf{- 3 5}$ | $\mathbf{- 4 0}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  |  |  |  |  |  |  |  |  |
| $\mathbf{e}_{\mathbf{i}}$ [mbar] | 6.108 | 4.015 | 2.597 | 1.652 | 1.032 | 0.633 | 0.380 | 0.223 | 0.128 |
| $\mathbf{e}_{\mathbf{w}}[\mathbf{m b a r}]$ | 6.108 | 4.212 | 2.857 | 1.905 | 1.246 | 0.799 | 0.502 | 0.308 | 0.184 |
| $\mathbf{U}_{\max }[\%]$ | $100 \%$ | $95 \%$ | $91 \%$ | $87 \%$ | $83 \%$ | $79 \%$ | $76 \%$ | $73 \%$ | $70 \%$ |
|  |  |  |  |  |  |  |  |  |  |

Tab. 5 : Maximum relative humidity values above ice

## Principles of Humidity - Dew Point, Frost Point

When you cool down air containing vapour below the saturation concentration the actual partial pressure e initially stays constant while the relative humidity is increasing due to the decrease of the saturation vapour pressure with temperature $t$.

$$
\begin{gathered}
U_{w}=\frac{e}{e_{w}} \cdot 100 \quad[\%] \\
\mathrm{t} \text { decreasing } \rightarrow \mathrm{e}_{\mathrm{w}}(\mathrm{t}) \text { decreasing } \rightarrow \mathrm{U}_{\mathrm{w}} \text { increasing }
\end{gathered}
$$

At the "dew point temperature $\mathbf{t}_{\mathbf{d}}$ " the saturation vapour pressure equals the actual vapour pressure i.e. $\mathrm{e}_{\mathrm{w}}\left(\mathrm{t}_{\mathrm{d}}\right)=\mathrm{e}$ and the relative humidity reaches its maximum value of $\mathrm{U}_{\mathrm{w}}=100 \%$.

The dew point temperature $t_{d}$ is therefore the temperature to which you have to cool down moist air at constant pressure for beginning condensation. It can be calculated from the temperature and relative humidity using the Magnus formula :

$$
\begin{gathered}
\mathrm{t}\left[{ }^{\circ} \mathrm{C}\right] \rightarrow \text { saturation vapour pressure } \mathrm{e}_{\mathrm{w}} \\
\mathrm{e}_{\mathrm{w}[\mathrm{mbar}], \mathrm{U}_{\mathrm{w}}[\%] \rightarrow e=\frac{e_{\mathrm{w}} \cdot U_{w}}{100}}^{\mathrm{e} \rightarrow t_{d}=T_{n} \cdot \frac{\ln \left(\frac{e}{A}\right)}{\left(m-\ln \left(\frac{e}{A}\right)\right)}}
\end{gathered}
$$

The Magnus parameters A, m, $\mathrm{T}_{\mathrm{n}}$ are given in Table 4 in the section "Magnus Formula".
Decreasing the temperature below the dew point temperature the partial vapour pressure exceeds the saturation value, so condensation occurs until the balance is reached again.

Below the triple point of water $\mathrm{t}<0.01^{\circ} \mathrm{C}$ you will usually find ice $\left(\mathrm{e}_{\mathrm{i}}\right)$ in your application instead of water $\left(\mathrm{e}_{\mathrm{w}}\right)$. The temperature at which the partial vapour pressure e reaches the saturation vapour pressure $e_{i}$ and frosting starts is called "frost point" $t_{f}>t_{d}$.

## Principles of Humidity - Absolute Humidity

## Absolute humidity $\mathrm{d}_{\mathrm{v}}\left[\mathrm{g} / \mathrm{m}^{3}\right]$

Gives the mass of water in $1 \mathrm{~m}^{3}$ moist air and can be calculated from the temperature t [ degC ] and the partial vapour pressure e [mbar] :
$t[\operatorname{deg} C] \rightarrow$ saturation vapour pressure $\mathrm{e}_{\mathrm{w}} \rightarrow \mathrm{e}=\mathrm{e}_{\mathrm{w}} \cdot \mathrm{U}_{\mathrm{w}}$

$$
d_{v}=216.7 \cdot\left(\frac{e}{273.15+t}\right)\left[\mathrm{g} / \mathrm{m}^{3}\right]
$$

## Principles of Humidity - Mixing ratio

## Mixing ratio r $[\mathrm{g} / \mathrm{kg}]$

Gives the mass of water you have to evaporate and mix with 1 kg dry air to perform a certain relative humidity $U_{w}$ or partial vapour pressure e
$t[\operatorname{degC}] \rightarrow$ saturation vapour pressure $\mathrm{e}_{\mathrm{w}} \rightarrow \mathrm{e}=\mathrm{e}_{\mathrm{w}} \cdot \mathrm{U}_{\mathrm{w}}$

$$
r=\frac{622 \cdot e}{(p-e)} \quad[g / k g]
$$

p air pressure [mbar]

## Principles of Humidity - Specific Enthalpy

## Specific enthalpy h[kJ/kg]

The specific enthalpie of air with temperature $t$, relative humidity $\mathrm{U}_{\mathrm{w}}$ and corresponding mixing ratio $r$ is the sum of the energies you need to create this state in the following way:
a) warming up 1 kg dry air from 0 degC to t
b) evaporating the vapour inside the moist air
c) warming up the vapour from $0 \operatorname{degC}$ to $t$

## $\rightarrow$ Specific enthalpie per 1 kg dry air:

$$
h=\left[c_{p a} \cdot t+\left(l_{w}+c_{p \cdot} \cdot t\right) \cdot r\right] \quad[k J / k g]
$$

$$
\begin{gathered}
\mathrm{c}_{\mathrm{pa}}=1.00545 \mathrm{~kJ} / \mathrm{kg} \quad \begin{array}{l}
\text { specific heat capacity of dry air at } \\
\text { constant pressure }
\end{array} \\
\mathrm{c}_{\mathrm{pv}}=1.85894 \mathrm{~kJ} / \mathrm{kg} \quad \begin{array}{c}
\text { specific heat capacity of vapour at } \\
\text { constant pressure }
\end{array} \\
\mathrm{I}_{\mathrm{w}}=2500.827 \mathrm{~kJ} / \mathrm{kg} \text { latent heat of water }
\end{gathered}
$$

The specific enthalpy is a relative quantity i.e. only differences are significant.
More generally enthalpy gives you the amount of energy which you need to bring moist air from a thermal state 1 into a state 2 .

## Example 1:

To warm up air from 20 to 25 degC and humidify the air from 40 to $60 \%$ relative humidity you will need $\mathrm{h}=20.2 \mathrm{~kJ} / \mathrm{kg}$.

## Example 2 :

Warming up air from 20 to 25 degC and keeping the relative humidity constant dissipates only $\mathrm{h}=10.3 \mathrm{~kJ} / \mathrm{kg}$.

## Example 3 :

When warming up air from 20 to 25 deg C and keeping the partial vapour pressure e constant ( $\mathrm{r}=$ constant, $\mathrm{t}_{\mathrm{d}}=$ constant ) the relative humidity decreases down to $\mathrm{U}_{\mathrm{w}}=29.5 \%$ which wastes only $\mathrm{h}=5.1 \mathrm{~kJ} / \mathrm{kg}$.

These examples are summarized in Table 6 and are drawn as "process 1, 2, 3" in Fig. 4 in the section "Mollier diagram".

| Example 1 | $\mathbf{t}$ <br> [degC] | $\mathbf{U}_{\mathbf{w}}[\%]$ | $\mathbf{h}[\mathbf{k J} / \mathbf{k g}]$ |
| :---: | :---: | :---: | :---: |
| state 1 | 20 | 40 | 34.6 |
| state 2 | 25 | 60 | 54.8 |
|  |  | difference | $\mathbf{2 0 . 2}$ |
| Example 2 | $\mathbf{t}$ <br> $[$ degC] | $\mathbf{U}_{\mathbf{w}}[\%]$ | $\mathbf{h}[\mathbf{k J / k g ]}$ |
| state 1 | 20 | 40 | 34.6 |
| state 2 | 25 | 40 | 44.9 |
|  |  | difference | $\mathbf{1 0 . 3}$ |
| Example 3 | $\mathbf{t}$ <br> $[$ degC] | $\mathbf{U}_{\mathbf{w}}[\%]$ | $\mathbf{h}[\mathbf{k J / k g ]}$ |
| state 1 | 20 | 40 | 34.6 |
| state 2 | 25 | 29.5 | 39.7 |
|  |  | difference | $\mathbf{5 . 1}$ |

Tab. 6: Enthalpy differences with different changes of state

## Principles of Humidity - Mollier diagram

Table 7 summarizes humidity function values at different temperatures. A Mollier diagram serves for solving problems in air conditioning technology graphically. It summarizes different humidity functions in one chart.

Using the mixing ratio $r$ there is a relation between $r$ and temperature $t$ with relative humidity $\mathrm{U}_{\mathrm{w}}$ as free parameter :

$$
r=\frac{622 \cdot e}{p-e} \rightarrow e=\frac{p \cdot r}{622+r}=\frac{e_{w}(t) \cdot U_{w}}{100}
$$

Using the Magnus formula you can draw a band of curves of constant relative humidity $\mathrm{U}_{\mathrm{w}}$ as functions $t(r)$ which is called "Mollier diagram". It is convenient to add curves of constant enthalpy to the Mollier diagram (as in Fig. 4) :

$$
\mathrm{h}=\left[\mathrm{c}_{\mathrm{pa}} \cdot \mathrm{t}+\left(\mathrm{l}_{\mathrm{w}}+\mathrm{c}_{\mathrm{pv}} \cdot \mathrm{t}\right) \cdot \mathrm{r}\right] \rightarrow \mathrm{t}=\left(\mathrm{h}-\mathrm{l}_{\mathrm{w}} \cdot \mathrm{r}\right) /\left(\mathrm{c}_{\mathrm{pa}}+\mathrm{c}_{\mathrm{p} v} \cdot \mathrm{r}\right)
$$

In this way you can describe graphically thermodynamical processes such as examples 1, 2, 3 in the section "Specific Enthalpy".

In a professional Mollier diagram usually further humidity functions are included.


Fig. 4 : Mollier diagram : curves of constant relative humidity and enthalpy. Examples 1, 2, 3 from the section "Specific Enthalpy" are drawn as processes 1, 2, 3.

Tab. 7: Humidity function values at different temperatures ( $p=1013.25 \mathrm{mbar}$, real gas corrections are taken into account) :

| $\mathbf{- 2 0}$ <br> $\mathbf{d e g C}$ |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| $\mathbf{U}_{\mathbf{w}}[\mathbf{\%}]$ | $\mathbf{t}_{\mathbf{d}}$ <br> $[\mathbf{d e g C}]$ | $\mathbf{e}$ <br> $[\mathbf{m b a r}]$ | $\mathbf{d}_{\mathbf{v}}$ <br> $\left[\mathbf{g} / \mathbf{m}^{3}\right]$ | $\mathbf{r}$ <br> $[\mathbf{g} / \mathbf{k g}]$ | $\mathbf{h}$ <br> $[\mathbf{k J} / \mathbf{k g}]$ |
| 80 | -22.56 | 1.013 | 0.867 | 0.622 | -18.56 |
| 70 | -24.07 | 0.886 | 0.758 | 0.544 | -18.76 |
| 60 | -25.78 | 0.759 | 0.650 | 0.467 | -18.95 |
| 50 | -27.78 | 0.633 | 0.542 | 0.389 | -19.14 |
| 40 | -30.17 | 0.506 | 0.433 | 0.311 | -19.34 |
| 30 | -33.17 | 0.380 | 0.325 | 0.233 | -19.53 |
| 20 | -37.26 | 0.253 | 0.217 | 0.155 | -19.72 |
| 10 | -43.90 | 0.127 | 0.108 | 0.078 | -19.92 |


| $\mathbf{0}$ degC |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| $\mathbf{U w}[\mathbf{\%}]$ | $\mathbf{t}_{\mathbf{d}}$ <br> $[\mathbf{d e g} \mathbf{C}]$ | $\mathbf{e}$ <br> $[\mathbf{m b a r}]$ | $\mathbf{d}_{\mathbf{v}}$ <br> $\left[\mathbf{g} / \mathbf{m}^{3}\right]$ | $\mathbf{r}$ <br> $[\mathbf{g} / \mathbf{k g}]$ | $\mathbf{h}$ <br> $[\mathbf{k J} / \mathbf{k g}]$ |
| 100 | 0.00 | 6.139 | 4.870 | 3.791 | 9.45 |
| 90 | -1.45 | 5.525 | 4.383 | 3.410 | 8.50 |
| 80 | -3.04 | 4.911 | 3.896 | 3.029 | 7.55 |
| 70 | -4.82 | 4.297 | 3.409 | 2.649 | 6.61 |
| 60 | -6.85 | 3.683 | 2.922 | 2.269 | 5.66 |
| 50 | -9.20 | 3.069 | 2.435 | 1.890 | 4.72 |
| 40 | -12.02 | 2.456 | 1.948 | 1.511 | 3.77 |
| 30 | -15.55 | 1.842 | 1.461 | 1.133 | 2.83 |
| 20 | -20.35 | 1.228 | 0.974 | 0.755 | 1.89 |
| 10 | -28.11 | 0.614 | 0.487 | 0.377 | 0.94 |
| 5 | -35.34 | 0.307 | 0.243 | 0.188 | 0.47 |


| $\mathbf{2 0}$ <br> $\mathbf{d e g} \mathbf{C}$ |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| $\mathbf{U}_{\mathbf{w}}$ <br> $[\mathbf{\%}]$ | $\mathbf{t}_{\mathbf{d}}$ <br> $[\mathbf{d e g C}]$ | $\mathbf{e}$ <br> $[\mathbf{m b a r}]$ | $\mathbf{d}_{\mathbf{v}}$ <br> $\left.\mathbf{[ g} / \mathbf{m}^{3}\right]$ | $\mathbf{r}$ <br> $[\mathbf{g} / \mathbf{k g}]$ | $\mathbf{h}$ <br> $[\mathbf{k J} / \mathbf{k g}]$ |
| 100 | 20.00 | 23.431 | 17.318 | 14.723 | 56.64 |
| 90 | 18.31 | 21.088 | 15.586 | 13.220 | 52.96 |
| 80 | 16.44 | 18.745 | 13.854 | 11.723 | 49.28 |
| 70 | 14.36 | 16.402 | 12.123 | 10.234 | 45.62 |
| 60 | 12.00 | 14.059 | 10.391 | 8.751 | 41.95 |
| 50 | 9.26 | 11.715 | 8.659 | 7.276 | 38.30 |
| 40 | 5.98 | 9.372 | 6.927 | 5.807 | 34.65 |
| 30 | 1.88 | 7.029 | 5.195 | 4.345 | 31.00 |
| 20 | -3.67 | 4.686 | 3.464 | 2.890 | 27.36 |
| 10 | -12.60 | 2.343 | 1.732 | 1.442 | 23.73 |
| 5 | -20.89 | 1.172 | 0.866 | 0.720 | 21.92 |


| $\mathbf{4 0}$ <br> $\mathbf{d e g C}$ |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| $\mathbf{U}_{\mathbf{w}}$ <br> $[\mathbf{\%}]$ | $\mathbf{t}_{\mathbf{d}}$ <br> $[\mathbf{d e g C}]$ | $\mathbf{e}$ <br> $[\mathbf{m b a r}]$ | $\mathbf{d}_{\mathbf{v}}$ <br> $\left.\mathbf{g} / \mathbf{m}^{3}\right]$ | $\mathbf{r}$ <br> $[\mathbf{g} / \mathbf{k g}]$ | $\mathbf{h}$ <br> $[\mathbf{k J} / \mathbf{k g}]$ |
| 100 | 40.00 | 74.052 | 51.237 | 49.041 | 158.72 |
| 90 | 38.04 | 66.647 | 46.113 | 43.791 | 146.57 |
| 80 | 35.89 | 59.242 | 40.989 | 38.623 | 134.49 |
| 70 | 33.48 | 51.836 | 35.866 | 33.535 | 122.47 |
| 60 | 30.76 | 44.431 | 30.742 | 28.525 | 110.52 |
| 50 | 27.61 | 37.026 | 25.618 | 23.590 | 98.64 |
| 40 | 23.84 | 29.621 | 20.495 | 18.730 | 86.83 |
| 30 | 19.14 | 22.216 | 15.371 | 13.943 | 75.08 |
| 20 | 12.79 | 14.810 | 10.247 | 9.226 | 63.39 |
| 10 | 2.62 | 7.405 | 5.124 | 4.579 | 51.77 |
| 5 | -6.78 | 3.703 | 2.562 | 2.281 | 45.99 |


| $\mathbf{6 0}$ <br> $\mathbf{d e g C}$ |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| $\mathbf{U}_{\mathbf{w}}$ <br> $[\mathbf{\%}]$ | $\mathbf{t}_{\mathbf{d}}$ <br> $\mathbf{d e g C}]$ | $\mathbf{e}$ <br> $[\mathbf{m b a r}]$ | $\mathbf{d}_{\mathbf{v}}$ <br> $\left[\mathbf{g} / \mathbf{m}^{3}\right]$ | $\mathbf{r}$ <br> $[\mathbf{g} / \mathbf{k g}]$ | $\mathbf{h}$ <br> $[\mathbf{k J} / \mathbf{k g}]$ |
| 100 | 60.00 | 200.610 | 130.470 | 153.543 | 400.02 |
| 90 | 57.74 | 180.549 | 117.423 | 134.859 | 363.59 |
| 80 | 55.26 | 160.488 | 104.376 | 117.055 | 327.75 |
| 70 | 52.50 | 140.427 | 91.329 | 100.069 | 292.48 |
| 60 | 49.38 | 120.366 | 78.282 | 83.846 | 257.75 |
| 50 | 45.79 | 100.305 | 65.235 | 68.337 | 223.57 |
| 40 | 41.51 | 80.244 | 52.188 | 53.494 | 189.91 |
| 30 | 36.17 | 60.183 | 39.141 | 39.276 | 156.77 |
| 20 | 28.99 | 40.122 | 26.094 | 25.644 | 124.14 |
| 10 | 17.51 | 20.061 | 13.047 | 12.563 | 91.99 |
| 5 | 6.97 | 10.030 | 6.523 | 6.219 | 76.10 |

## Principles of Humidity - Literature

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